



Buckled elastic sheet as a vortex generator in dual channels

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(Received 14 July 2023; revised 19 February 2024; accepted 5 March 2024)

This study presents a dual-channel vortex generator (VG) that leverages the snap-through behaviour of flexible sheets. The VG outperforms a similar-sized rigid VG in generating vortices within dual-channel flows while minimizing pressure loss. Numerical simulations using the immersed boundary-lattice Boltzmann method analyse the dynamics and vortex generation performance of the sheet under various system parameters. Two distinct modes are identified for the elastic sheet: a sustained snap-through mode (SSTM) and a dormant mode (DM). The sheet's mode is predominantly influenced by its length ratio (L^*) , bending stiffness (K_h^*) and flow strength, with the mass ratio having a minimal impact. The sheet exhibiting regular SSTM can effectively generate vortices in both channels and the vortex generation performance can be conveniently tuned by altering the sheet's initial buckling (i.e. L^*). An increase in K_b^* results in a higher critical Reynolds number (Re_c) required for mode transition. An increase in L*, however, initially raises Re_c and then lowers it, suggesting an optimal length ratio (approximately 0.7 for our considered system) for minimizing the Re_c necessary to trigger SSTM. Furthermore, a disparity in the flow strength between channels is found to suppress the snap-through of the sheet; a greater disparity, however, is permissible to induce the SSTM of more compliant sheets. These findings underscore the potential of snap-through behaviour for enhanced flow manipulation in dual-channel systems.

Key words: flow-structure interactions, mixing enhancement

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1. Introduction

Enhancing flow mixing and improving heat transfer efficiency are desired across diverse industrial applications, including chemical processing, food industries, power generation, refrigeration and thermal management in electronic devices (Moore & Shi 2014; Lee *et al.* 2016; Cai *et al.* 2017; Zhang, Wang & Yan 2021; Liao & Jing 2023*a*). Vortex generators (VGs) offer a practical approach to address these demands. By strategically placing these small devices on heat transfer surfaces, VGs generate vortices and modify flow characteristics. The induced vortices promote flow mixing, disrupting stagnant regions and promoting even fluid distribution over the heat transfer surface. This even distribution allows a larger portion of the surface to be actively involved in heat transfer, leading to efficient thermal exchange and minimized thermal gradients (Awais & Bhuiyan 2018).

Numerous studies have investigated the effectiveness of different types of VGs in augmenting heat transfer in channel or pipe flows. Commonly used VGs comprise rigid structures affixed to wall surfaces, manifesting in diverse configurations, including ribs (Webb, Eckert & Goldstein 1971; Han, Glicksman & Rohsenow 1978; Kim et al. 2011; Tanda 2011; Mahmoodi-Jezeh & Wang 2020), fins (Jeong et al. 2014; Zhao et al. 2016; Hussain et al. 2019), twisted tapes (Bharadwaj, Khondge & Date 2009; Bhattacharyya 2020) and delta winglets (He et al. 2012; Zhou & Feng 2014; Akcayoglu & Nazli 2018; Skullong et al. 2018; Wu et al. 2022b), among others. Each type induces unique flow patterns and enhances heat transfer through different mechanisms. Ribs and fins mounted on heat transfer surfaces disrupt the boundary layer and generate vortices, promoting heat transfer by increasing the turbulence intensity and enhancing convective heat transfer coefficients. Twisted tapes, however, are characterized by their helical shapes. They create swirl flows and induce secondary flow patterns, leading to enhanced heat transfer through improved mixing and disruption of the thermal boundary layer. Delta winglets, with their triangular shape, generate vortices and induce flow separation and reattachment. This enhances heat transfer by disrupting the boundary layer and improving convective heat transfer through increased fluid motion and thermal contact with the surface.

While rigid VGs offer significant benefits in enhancing flow mixing and heat transfer, they also have inherent shortcomings, such as limited flexibility, significantly increased pressure drop, higher energy consumption and reduced overall system efficiency (Promvonge & Thianpong 2008). Flexible VGs, however, are promising alternatives due to their inherent flexibility or adaptability (Gallegos & Sharma 2017). Unlike rigid VGs, which are fixed structures, flexible VGs have the ability to deform, adjust or change their shape in response to varying flow conditions. These innovative devices harness the flapping motions of flexible structures to induce vigorous vortex shedding, promoting intense flow mixing and thereby enhancing convective heat transfer. The flexibility also empowers them to optimize flow disturbance and minimize flow resistance (Khatavkar et al. 2007; Lambert & Rangel 2010; Chen et al. 2020; Liao & Jing 2023b). Shoele & Mittal (2014) introduced a novel method for generating vortices in a heated channel using a flexible reed. The reed was clamped at its leading edge while leaving the trailing edge free, resulting in a configuration known as the conventional flag model. This unique configuration demonstrates an exceptional thermal efficiency factor exceeding 120%. Inverted flags clamped at the trailing edge (Park et al. 2016; Yu, Liu & Chen 2018; Chen et al. 2019) have also been recognized as highly effective flexible VGs. Research has shown that the presence of inverted flags can lead to a remarkable 2.5-fold improvement in heat removal at a Reynolds number (Re) of 800, at the cost of an appreciable increase in pressure drop (Park et al. 2016). Researchers have also explored the use of wall-mounted flags as VGs in channel flows. Lee et al. (2017) and Lee, Park & Sung (2018) conducted numerical simulations to investigate the dynamics of a pair of wall-mounted flexible flags, and their effects on downstream vortical structures and heat transfer enhancement in a Poiseuille channel flow. Chen *et al.* (2020) extended this research by considering scenarios involving multiple wall-mounted flexible flags as VGs. In another study, Singh & Lakkaraju (2019) numerically characterized the flow behaviour when flexible plates were anchored to opposite walls of a channel. Their findings reveal that wall-mounted flexible plates induce early flow instabilities, resulting in enhanced flow mixing levels. These investigations contribute to a deeper understanding of using flexible flags/plates as VGs to enhance flow mixing and improve heat transfer in channel flows.

The snap-through phenomenon of elastic sheets has recently gained considerable attention (Cao *et al.* 2021). Snap-through refers to a phenomenon in which an elastic sheet undergoes a sudden and rapid transition from one stable configuration to another. This transition is characterized by a sudden change in shape and a significant release of stored energy within the sheet. It occurs when the applied load or deformation exceeds a critical threshold, causing the sheet to 'snap' or buckle into a new configuration. The snap-through behaviour of elastic sheets has found applications in various fields, including deployable structures (Bobbert, Janbaz & Zadpoor 2018; Arnouts *et al.* 2019; Yeow *et al.* 2021), robotics (Currier, Lheron & Modarres-Sadeghi 2020; Gorissen *et al.* 2020; Dong *et al.* 2022; Wu et al. 2022a), flow control (Gomez, Moulton & Vella 2017; Jiao & Liu 2021; Zhang *et al.* 2022) and energy harvesting devices (Qin *et al.* 2019; Zhou *et al.* 2019; Kim *et al.* 2020; Wang *et al.* 2021, 2023). By harnessing the abrupt configuration changes, engineers and researchers can exploit the unique properties and functionalities associated with snap-through behaviour to design innovative and efficient systems.

Prior research in vortex generator designs predominantly targeted single-channel structures. This study introduces a novel flexible VG that is specifically designed for dual-channel flow configurations. In contrast to traditional flapping flag-type VGs, the proposed design capitalizes on the snap-through behaviour of elastic sheets, offering exceptional capabilities for vortex generation and flow manipulation within dual-channel flows. This unique design enables rapid and reversible transitions between different stable configurations, leading to the creation of powerful vortices and enhanced flow disturbances in both channels. The dynamics of the sheet, the characteristics of vortex generation and the influence of governing parameters on the system are thoroughly investigated using numerical simulations. The concept may contribute to the advancement of flow control strategies and open new possibilities for optimizing flow characteristics in dual-channel flow configurations. The findings may shed light on the potential of using snap-through behaviour in elastic sheets as an effective means of achieving enhanced flow manipulation and vortex generation. The paper is organized as follows. Section 2 provides a description of the physical problem and outlines the methodology employed. In § 3, detailed results are presented, analysed and discussed. Finally, § 4 offers concluding remarks based on the findings.

2. Physical problem and methodology

2.1. Problem description

Figure 1 illustrates our proposed VG for dual channels. The dual channels considered in this study are symmetrical, sharing a middle dividing wall and possessing identical dimensions. Each channel has an identical width of H. A buckled elastic sheet with a length of L (L = 2H) is clamped at the mid-wall, functioning as a VG for the dual-channel system. The ends of the sheet are clamped parallel to the flow direction a distance of d



Figure 1. Schematic diagram for the dual channel-VG system. The sheet is initially buckled and clamped horizontally at the mid-wall of two identical channels. The sheet has a length of L when it is intrinsically straight and its end-to-end distance is d after buckling. The dimensions of the two channels are 12L in length and 0.5L in height.

apart, which also determines the sheet's initial buckling. The leading end of the sheet is located at a position *Le* downstream from the channel inlet. Two uniform flows of the same fluid enter the channels from the inlet with velocities U_1 and U_2 , pass over the sheet, and leave from the outlet. When the flows reach sufficient strength, they can initiate a snap-through oscillation of the sheet, leading to the formation of vortices and significant flow disturbances downstream.

In this study, the problem is considered in a two-dimensional (2-D) framework. It is assumed that all channel walls are rigid and there is no leakage at the walls or the sheet. Therefore, the fluids in the two adjacent channels are completely separated and they interact with each other only through the clamped elastic sheet. To begin with, the sheet is buckled downwards at equilibrium. Two observation points are respectively defined at the centreline of each channel to measure velocity fluctuations in the near and far wakes of the channels.

2.2. Mathematical formulation and numerical method

The flow is assumed to be incompressible and Newtonian in this study. Its governing equations are given as follows:

$$\nabla \cdot \boldsymbol{u} = \boldsymbol{0}, \tag{2.1}$$

$$\rho\left(\frac{\partial \boldsymbol{u}}{\partial t} + \boldsymbol{u} \cdot \boldsymbol{\nabla} \boldsymbol{u}\right) = -\boldsymbol{\nabla} p + \mu \Delta \boldsymbol{u} + \boldsymbol{f}, \qquad (2.2)$$

where u = (u,v) is the flow velocity vector, p the pressure and f the body force term. The flow Reynolds number is defined as $Re = \rho HU/\mu$, where ρ is the fluid density and μ is the dynamic viscosity. Here, U represents the inlet velocity, which is U_1 for Channel 1 and U_2 for Channel 2. Additionally, H = 0.5L is the width of a single channel.

The sheet is assumed to be two-dimensional and thin. Its dynamics is governed by the following nonlinear partial differential equation (Connell & Yue 2007; Hua, Zhu & Lu 2013):

$$\rho_s \frac{\partial^2 X}{\partial t^2} = \frac{\partial}{\partial s} \left[Eh \left(1 - \left(\frac{\partial X}{\partial s} \cdot \frac{\partial X}{\partial s} \right)^{-1/2} \right) \frac{\partial X}{\partial s} - \frac{\partial}{\partial s} \left(K_b \frac{\partial^2 X}{\partial s^2} \right) \right] + F, \quad (2.3)$$

where X is the position vector of the sheet and s is the Lagrangian coordinate along the sheet. The first and second terms on the right-hand side of the equation calculate the tensile force and bending force, respectively; K_b and Eh denote the bending and stretching

stiffnesses of the sheet, respectively; F is the Lagrangian force exerted on the sheet by the neighbouring fluid and ρ_s is the linear density of the sheet.

Equations (2.1)–(2.3) are non-dimensionalized using the following characteristic scales: *L* for length, U_1 for velocity, L/U_1 for time, ρ for density, ρL for linear density, ρU_1^2 for pressure, $\rho U_1^2/L$ for force density, $\rho U_1^2 L^3$ for bending stiffness and $\rho U_1^2 L$ for stretching stiffnesses. The dimensionless forms of (2.1)–(2.3) are

$$\nabla^* \cdot \boldsymbol{u^*} = 0, \tag{2.4}$$

$$\frac{u^{*}}{t^{*}} + u^{*} \cdot \nabla^{*} u^{*} = -\nabla^{*} p^{*} + \frac{0.5}{Re} \nabla^{*2} u^{*} + f^{*}, \qquad (2.5)$$

$$m^* \frac{\partial^2 X^*}{\partial t^{*2}} = \frac{\partial}{\partial s^*} \left[Eh^* \left(1 - \left(\frac{\partial X^*}{\partial s^*} \cdot \frac{\partial X^*}{\partial s^*} \right)^{-1/2} \right) \frac{\partial X^*}{\partial s^*} - \frac{\partial}{\partial s^*} \left(K_b^* \frac{\partial^2 X^*}{\partial s^{*2}} \right) \right] + F^*,$$
(2.6)

 $\frac{\partial}{\partial t}$

where the quantities with an asterisk (*) represent their non-dimensional counterparts. Thus, we have the following dimensionless parameters for the sheet: the mass ratio $m^* = \rho_s/\rho L$, the bending stiffness $K_b^* = K_b/\rho U_1^2 L^3$, the stretching stiffnesses $Eh^* = Eh/\rho U_1^2 L$ and the length ratio $L^* = d/L$, which defines the initial buckling of the sheet.

In the present study, the flow dynamics is solved by a multi-relaxation-time lattice Boltzmann model (MRT-LBM) due to its efficiency and parallelization (Kang 2010; Wang *et al.* 2016*a*,*b*, 2017*a*,*b*; Wang & Tang 2018, 2019; Cui *et al.* 2022*a*). The evolution equation of the MRT-LBM with an external force term is given as

$$f_{\alpha}(\boldsymbol{x} + \boldsymbol{e}_{\alpha}\Delta t, t + \Delta t) - f_{\alpha}(\boldsymbol{x}, t)$$

= $-\boldsymbol{M}^{-1}SM(f_{\alpha}(\boldsymbol{x}, t) - f_{\alpha}^{eq}(\boldsymbol{x}, t)) - \boldsymbol{M}^{-1}\left(\boldsymbol{I} - \frac{\boldsymbol{S}}{2}\right)MF_{\alpha}(\boldsymbol{x}, t)\Delta t,$ (2.7)

where $f_{\alpha}(\mathbf{x}, t)$ is the density distribution function of particles at position \mathbf{x} and time t with velocity \mathbf{e}_{α} ; \mathbf{M} is a transformation matrix and \mathbf{S} is a non-negative diagonal relaxation matrix. Additionally, $F_{\alpha}(\mathbf{x}, t)$ accounts for the effect of external forces and can be calculated by (Premnath & Abraham 2007)

$$F_{\alpha}(\boldsymbol{x},t) = \frac{[\boldsymbol{e}_{\alpha} - \boldsymbol{u}(\boldsymbol{x},t)]\boldsymbol{f}(\boldsymbol{x},t)}{\rho c_{s}^{2}} f_{\alpha}^{eq}(\boldsymbol{x},t), \qquad (2.8)$$

where c_s is the model's speed of sound and $f_{\alpha}^{eq}(\mathbf{x}, t) = \omega_{\alpha} \rho [1 + \mathbf{e}_{\alpha} \cdot \mathbf{u}/c_s^2 + (\mathbf{e}_{\alpha} \cdot \mathbf{u})^2/2c_s^4 - \mathbf{u}^2/2c_s^2]$ is the equilibrium distribution function with ω_{α} being the weighting coefficients. The velocity \mathbf{u} , mass density ρ and pressure p of the fluid can be calculated by

$$\rho = \sum_{\alpha} f_{\alpha}, \quad \boldsymbol{u} = \left(\sum_{\alpha} \boldsymbol{e}_{\alpha} f_{\alpha} + \frac{\boldsymbol{f}}{2} \Delta t\right) / \rho, \quad \boldsymbol{p} = c_s^2 \rho. \quad (2.9a-c)$$

The sheet is discretized into a collection of Lagrangian points that are uniformly distributed and its dynamics is solved using a finite-difference method (Huang, Shin & Sung 2007; Yuan *et al.* 2014). Specifically, the tensile force is computed at the centres of the segments, while the bending force is evaluated at the Lagrangian points. In our simulations, we use a sufficiently large *Eh* value to ensure that the sheet exhibits near inextensibility, with the maximal elongation rate controlled below 0.5%.

The momentum-exchange-based immersed boundary method (IBM) is employed to handle the interaction between the fluid and the sheet. In this method, the hydrodynamic force exerted on the sheet is evaluated by (Niu *et al.* 2006)

$$F(X,t) = \sum_{\alpha} \boldsymbol{e}_{\alpha} \ [f_{\alpha}(X,t+\Delta t) - f_{-\alpha}(X,t)], \tag{2.10}$$

where $-\alpha$ denotes the opposite direction of α and $f_{\alpha}(X, t + \Delta t) = \int_{\Omega} f_{\alpha}(x, t + \Delta t)$ $\delta(x - X(s, t)) dx$ is the bounce-back distribution function of $f_{-\alpha}(X, t)$. The reaction force of F(X, t) is spread to the nearby fluid points as follows to enforce the no-slip condition:

$$f(\mathbf{x},t) = \int_{\Gamma} -F(\mathbf{X},t)\delta(\mathbf{x} - \mathbf{X}(s,t)) \,\mathrm{d}s, \qquad (2.11)$$

where Γ and Ω denote the fluid and solid domains, respectively, and δ is the Dirac delta function (Peskin 2002; Yang *et al.* 2009).

2.3. Output variables and boundary conditions

In our simulations, we specify a large value of Eh^* to enforce the inextensibility condition of the sheet. When analysing the motion characteristics of the thin sheet, our focus will be on several dimensionless coefficients: lift coefficient (C_l) , drag coefficient (C_d) , kinetic energy coefficient (E_b^*) and potential energy coefficient (E_k^*) . These coefficients are defined as follows:

$$C_{l} = \frac{F_{l}}{0.5\rho U_{1}^{2}L}, \quad C_{d} = \frac{F_{d}}{0.5\rho U_{1}^{2}L}, \quad E_{b}^{*} = \frac{E_{b}}{0.5\rho U_{1}^{2}L^{2}}, \quad E_{k}^{*} = \frac{E_{k}}{0.5\rho U_{1}^{2}L^{2}}, \quad (2.12a-d)$$

where F_l and F_d are the lift and drag forces exerted on the sheet, while $E_b = 0.5K_b \int_0^L (\partial^2 X/\partial s^2)^2 ds$ and $E_k = 0.5\rho_s \int_0^L (\partial X/\partial t)^2 ds$ represent the sheet's bending and kinetic energies.

When analysing the system's performance, the following statistically derived physical quantities will be considered:

$$\overline{C_d}, \overline{E_b^*}, \overline{E_k^*}, \sigma(C_l), \sigma(v^*),$$
(2.13)

where $\overline{C_d}$, $\overline{E_b^*}$ and $\overline{E_k^*}$ represent the time-averaged values of C_d , E_b^* and E_k^* , respectively; $\sigma(C_l)$ and $\sigma(v^*)$ refer to the standard deviation of C_l and v^* , respectively.

In this study, we strategically position the vortex generator near the channel inlet to maximize its effect on the downstream regions. Accordingly, our simulations implement a uniform velocity boundary condition at the channel inlets. The channel walls are subjected to a no-slip condition. At the channel outlet, we specify a pressure boundary condition to account for potential backflow. Oscillations of the sheet may result in volume fluctuations within each channel. The pressure boundary at the outlet can effectively addresses the potential compressibility issues arising from these fluctuations, as has previously demonstrated by Huang *et al.* (2021) and Luo *et al.* (2008) in simulating incompressible flows in collapsible channels.

The sheet's end-to-end distance (d) is varied to change its initial buckling (i.e. the length ratio $L^* = d/L$) in this study. However, with a given value for d, the initial buckled shape of the sheet remains unknown. To determine it, we first run the structural solver independently, applying a fixed boundary condition at one end of the sheet and a moving

Grid resolutions	Δp^* at the lower channel	Δp^* at the upper channel	$\overline{C_d}$	$\overline{E_b^*}$
$\Delta x = L/80$	1.280	1.130	0.793	0.137
$\Delta x = L/120$	1.272	1.215	0.820	0.134
$\Delta x = L/180$	1.275	1.237	0.822	0.135
Table 1. Results for	or the grid independence study at	system parameter: $Re_1 = Re_2 = 1$	1000, $K_h^* = 5$	$\times 10^{-3}$,

 $L^* = 0.8$, $Le^* = 3$ and $m^* = 1$.

boundary condition at the opposite end (i.e. sliding the opposite end towards the fixed end). The fluid–structure interaction simulation is started after we obtain the initial buckled shape, during which the two ends of the sheet are imposed with a clamped boundary condition, i.e.

$$X = X(s, 0), \quad \frac{\partial X}{\partial s} = (1, 0), \quad \text{at } s = 0,$$
 (2.14)

$$X = X(s, 0), \quad \frac{\partial X}{\partial s} = (-1, 0) \text{ at } s = L.$$
 (2.15)

2.4. Numerical validations and grid independence study

The simulations were performed using our in-house code which has been thoroughly validated and verified in our previous studies (Cui *et al.* 2019, 2022*b*; Cui, Liu & Jin 2021). In our simulations, we set the Eulerian grid spacing Δx to be 1.5 times the Lagrangian grid spacing Δs (i.e. $\Delta x = 1.5 \Delta s$). A grid independence study is conducted to ensure grid convergence, using the following system parameters: $Re_1 = Re_2 = 1500$, $K_b^* = 5 \times 10^{-3}$, $L^* = 0.8$, $Le^* = 3$ and $m^* = 1$. In each test case, the grid spacing is refined 1.5 times more than the coarser level. Additionally, the supporting range of the Dirac delta function is also expanded by 1.5 times to maintain a constant effective thickness of the sheet throughout each refinement (Wiens & Stockie 2015). After comparing the pressure drop (Δp^*) , $\overline{C_d}$ and $\overline{E_b^*}$ across various grid resolutions (refer to table 1), we determined that the solution achieves grid independence when $\Delta x = L/120$.

3. Results and discussion

This section presents, analyses and discusses the detailed results. We begin by analysing the sheet dynamics and vortex generation characteristics in a baseline case where the sheet undergoes a sustained snap-through oscillation. Subsequently, we investigate the influence of the bending stiffness (K_b^*) , length ratio (L^*) , mass ratio (m^*) and sheet position (Le^*) on the sheet dynamics and vortex generation. Lastly, we discuss the Reynolds number (Re) effect and determine the critical flow conditions required to initiate the snap-through oscillation of the sheet in two scenarios: whether $Re_1 = Re_2$ or $Re_1 \neq Re_2$. Unless otherwise stated, it is assumed that the flows in the upper and lower channels have the same Re.

3.1. Sheet dynamics and vortex generation

In this study, two distinct modes are identified for the elastic sheet: a sustained snap-through mode (SSTM) and a dormant mode (DM). The SSTM is characterized by



Figure 2. (a) Sheet dynamics in a typical snapping cycle. Left: Superimposed sheet profiles throughout one snapping cycle. Right: Sequential presentation of the decomposed motion, highlighting the step-by-step progression. (b) Time evolution of the vertical coordinate of the sheet's midpoint (Y_m^*) , the sheet's bending energy (E_b^*) and kinetic energy (E_k^*) in an SSTM case. System parameters: $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$.

the sheet repeatedly snapping from one channel to the other at a relatively low frequency, as illustrated in supplementary movie 1 available at https://doi.org/10.1017/jfm.2024.244. This mode is self-excited, induced by a synergistic interaction between the sheet's motion and aero/hydrodynamic forces (Mao, Liu & Sung 2023). DM involves the sheet exhibiting rapid yet minor vibrations within one channel without crossing the mid-wall of the dual channels, as shown in supplementary movie 2.

Figure 2(a) depicts the dynamics of the sheet in a typical snapping cycle. Both the sheet motion and the flow patterns exhibit a quasi-periodic state after 3–5 sheet oscillation



Figure 3. (a) Vortex generation and (b) u-velocity contour for a rigid stationary sheet (top row) and a snapping elastic sheet (rows 2–6). System parameters: $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$.

cycles. The superimposed sheet profiles on the left are symmetrical about the line between the two clamped ends. The snapping cycle consists of two distinct stages: snap-up and snap-down. The snap-up stage begins with the sheet undergoing an upward stroke due to the generated transverse forces. During this process, the sheet's front half is observed to get transversely lifted before its rear half. The upward stroke is followed by a streamwise shift along the flow direction demonstrating the drag force of the fluid. Shortly after, there is an anti-streamwise movement driven by the restoring force generated within the sheet, seeking to bring the sheet back to its energy-minimized equilibrium position. These shifts occur swiftly, constituting only approximately 13 % of the entire cycle, and a rapid release and storage of bending and kinetic energies occur during these shifts, as depicted in figure 2(b). The stage concludes with damped oscillations of diminishing amplitude. Similarly, the snap-down stage follows the same pattern as snap-up, but starts with a downward stroke. The upward and downward strokes transpire at a relatively gradual pace, taking up approximately 70% of the cycle's duration. Consequently, the time-averaged kinetic energy of the sheet (E_k^*) over one cycle is considerably lower (nearly an order of magnitude lower) than the bending energy (E_h^*) . Prior to crossing the mid-wall, the sheet experiences a much slower transverse movement. Upon reaching and subsequently crossing the mid-wall, there is a sharp increase in the velocity of the transverse motion, which is accompanied by a rapid decrease in bending energy and a swift increase in kinetic energy (figure 2b).

Figure 3 shows a series of snapshots highlighting the vortex structures and *u*-velocity contours for both our proposed VG and a comparably sized rigid sheet featuring a protruding profile. In the rigid-sheet scenario, vortices are intermittently formed, predominantly in the lower channel. In contrast, the elastic sheet dynamically generates a vibrant spectrum of vortices across both upper and lower channels (see supplementary movie 3), underscoring its heightened sensitivity and adaptability to fluid interactions

	$\sigma(v^*)$						Δp^*		
	Near wake			Far wake					
Туре	Lower channel	Upper channel	Average	Lower channel	Upper channel	Average	Lower channel	Upper channel	Average
Elastic	0.61	0.58	0.60	0.44	0.40	0.42	1.21	1.16	1.19
Rigid	1.02	2.76×10^{-3}	0.51	0.80	1.88×10^{-4}	0.40	2.57	0.62	1.60
Table 2.	A compa sheets. A	arison of the vo Additional syst	ortex genera em parame	ation perfo eters: <i>Re</i> 1 =	$rmance betwee = Re_2 = 1000, I$	en the elast $L^* = 0.75, I$	ic $(K_b^* = 3$	5×10^{-3}) $4 m^* = 1.$	and rigid

(figure 3*a*). While the rigid sheet induces a fairly consistent flow with minimal disturbances, the elastic sheet, particularly when snapping, introduces a complex tapestry of velocity variations, suggesting its capability for more refined flow manipulations, as depicted in figure 3(*b*). A more qualitative analysis comparing the vortex generation capabilities of these two configurations can be found in table 2. Compared with the rigid counterpart, the elastic case augments the $\sigma(v^*)$ by an appreciable 17.6% in the near-wake region and 5% in the far-wake region. Moreover, the elastic case experiences a significant reduction in pressure drop, averaging 25.6% overall and reaching 52.9% in the lower channel. These findings highlight the potential advantages of incorporating the snap-through behaviour of elastic sheets in dual-channel systems for improved vortex generation and flow mixing.

3.2. Effects of bending stiffness

We then analysed the influence of bending stiffness (K_b^*) on the dynamics of the elastic sheet and its vortex generation performance. The bending stiffness was varied from 6.25×10^{-4} to 2×10^{-2} , covering a range that allowed observation of diverse dynamical behaviours. This investigation was conducted with a fixed set of system parameters: $Re_1 = Re_2 = 1000$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$.

Figure 4 offers a detailed overview of the dynamic evolution of a buckled elastic sheet under various K_b^* values. Varying the K_b^* value reveals two distinct sheet modes: the SSTM occurs at $K_b^* \leq 5 \times 10^{-3}$ and the DM at $K_b^* \geq 1 \times 10^{-2}$. The superimposed sheet profiles in figure 4(*a*) vividly illustrate the dynamic morphological changes of the elastic sheet at different K_b^* values. With a low bending stiffness ($K_b^* = 6.25 \times 10^{-4}$), the sheet is highly compliant, and thus demonstrates heightened sensitivity to the aero/hydrodynamical load. As a result, a chaotic and rather irregular snap-through oscillation is observed. Within a medium bending stiffness range $(1.25 \times 10^{-3} \leq K_b^* \leq 5 \times 10^{-3})$, the superimposed profiles of the sheet are more structured and symmetrically aligned. These are referred to as 'regular snap-through oscillations', which, as will be demonstrated later, are more favourable in vortex generations. Additionally, as shown in figure 4(*b*), an increase in the K_b^* value results in a more pronounced bulbous central region. In the SSTM, there is a mild increase in the oscillation amplitude of Y_m^* (*A**) with rising K_b^* values (figure 4*b*). The snapping frequency, however, initially increases and then decreases as K_b^* increases (figure 4*c*), a pattern consistent with the numerical results of Mao *et al.* (2023) under uniform flow conditions. The turning point in this process occurs at $K_b^* = 1.25 \times 10^{-3}$, beyond which the sheet exhibits regular snap-through oscillation (figure 4*a*). A higher

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Figure 4. Sheet dynamics and associated metrics for varied K_b^* values. (*a*) Sequentially superimposed sheet profiles, demonstrating morphological changes across different K_b^* values. (*b*) Variation of the oscillation amplitude of Y_m^* (A^*) across the range of K_b^* , delineating two regimes: SSTM and DM. (*c*) Snapping frequencies presented for the SSTM cases. (*d*) Plots of $\overline{C_d}$ and $\sigma(C_l)$ showing their dependence on K_b^* . (*e*) Energy metrics, $\overline{E_b^*}$ and $\overline{E_k^*}$, plotted against K_b^* . Relevant system parameters: $Re_1 = Re_2 = 1000$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$.

snapping frequency is advantageous for achieving more synchronous flow mixing results between the two channels. Figure 4(d) shows how the average drag coefficient (\overline{C}_d) and the standard deviation of the lift coefficient $(\sigma(C_l))$ vary with K_b^* , while figure 4(e) depicts the variation of the sheet's mean bending energy (\overline{E}_b^*) and mean kinetic energy (\overline{E}_k^*) with changes in the K_b^* value. As K_b^* increases, both \overline{C}_d and \overline{E}_b^* rise, whereas $\sigma(C_l)$ and \overline{E}_k^* exhibit a decline. Combining the trends presented in figure 4(*b*-*e*), an increase in A^* correlates with an increase in both \overline{C}_d and \overline{E}_b^* , which in turn can lead to enhanced mixing effects, as will be elucidated in subsequent discussions. The variation in $\sigma(C_l)$ primarily influences the sheet's oscillation frequency and an increase in $\sigma(C_l)$ leads to a rise in \overline{E}_k^* ,



Figure 5. Characteristics of the flow field and associated metrics for varied K_b^* values. (a,b) Time-averaged vorticity field and v-velocity contours for select K_b^* values. (c) Variation of v-velocity fluctuation $\sigma(v^*)$ in both the near- and far-wake regions of the upper and lower channels. Averaged trends for the near-wake and far-wake regions are indicated with short dashed lines. (d) Evolution of the pressure drop Δp^* across the K_b^* range. Accompanying system parameters: $Re_1 = Re_2 = 1000 L^* = 0.75$, $Le^* = 3$ and $m^* = 1$.

which, in turn, affects the synchrony of the mixing effects between the channels. From figures 4(*b*) and 4(*d*), it is also found that when the sheet operates in the DM, it exhibits much lower values of A^* and $\sigma(C_l)$, and significantly higher values of $\overline{C_d}$ compared with those in the SSTM.

We also evaluated the vortex generation and flow mixing characteristics of the VG at various K_b^* values. Figure 5 shows the flow-field characteristics and some associated metrics from our simulations. In the dormant mode, the sheet generates vortices only in the lower channel, with barely any noticeable vortices and v-velocity (v^*) in the upper channel. However, in the sustained snap-through mode, the sheet produces equivalent vortex generation and v^* distribution in both channels, as shown in the time-averaged flow information in figure 5(a,b). The fluctuations of the v-velocity ($\sigma(v^*)$) at selected downstream positions (as referenced in figure 1) are illustrated in figure 5(c), where a higher $\sigma(v^*)$ value indicates enhanced flow mixing. The observed trend is that the average $\sigma(v^*)$ value initially rises with increasing K_b^* values, but subsequently drops as the sheet transitions from SSTM to DM. When K_b^* is within the range of 1.25×10^{-3} to

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 5×10^{-3} , the average $\sigma(v^*)$ value consistently exceeds that of the rigid case, suggesting that a sheet in regular SSTM can outperform a rigid VG in flow mixing. The optimal flow mixing performance, given our system parameters, occurs at $K_b^* = 2.5 \times 10^{-3}$. At this bending stiffness, both the disturbance at the boundary layer (figure 5*a*) and the v-velocity (figure 5*b*) are maximized. Figure 5(*d*) shows the evolution of the pressure drop Δp^* across the K_b^* range, capturing the general flow resistance trends in relation to K_b^* . In the DM cases, the lower channel, which houses the sheet, experiences a significantly greater pressure drop (over 2.5 times) than the upper channel. In contrast, the SSTM cases show no substantial difference in pressure drops between channels. In terms of the average pressure drop across both channels, it increases as the K_b^* value increases. Moreover, the dual channel with a sheet in SSTM displays a markedly reduced average pressure drop compared with scenarios with the sheet in DM, underscoring another advantage of using a snap-through sheet as a vortex generator in dual-channel configurations.

3.3. Effects of length ratio

The length ratio (L^*) is reported to play a pivotal role in influencing the snap-through oscillations of elastic sheets in a uniform flow (Kim *et al.* 2021*a*; Mao *et al.* 2023) and in the context of a single laminar channel flow (Wang *et al.* 2023). In this study, we examined the impact of L^* on the snap-through oscillations of elastic sheets in a dual-channel flow system, with a special focus on the sheet's vortex generation performance. The L^* value was varied between 0.6 and 0.9, where a smaller L^* value represents a more pronounced initial buckling and greater prestored bending energy. Other parameters considered in our analysis include $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $Le^* = 3$ and $m^* = 1$.

Figure 6 provides a comprehensive overview of how the dynamics of a buckled elastic sheet vary with different L^* values. As the L^* value increases, there is a notable decline in both the sheet's buckling degree and oscillation amplitude A^* (as seen in figures 6aand 6b). Once L^* exceeds 0.8, a transition from SSTM to MD occurs, resulting in a sharp decrease in A^* . The oscillation behaviour almost disappears in the case $L^*=0.9$, where the sheet exhibits the least initial buckling. In figure 6(c), the snapping frequencies for the SSTM cases are depicted. The frequencies initially increase and then decrease, with the peak frequency occurring at a medium initial buckling of $L^*=0.7$. As will be discussed later, excessively large or small initial buckling inhibits the occurrence of sustained snap-through oscillation. Figures 6(d) and 6(e) show a nearly linear decline in both $\overline{C_d}$ and $\overline{E_b^*}$ as L^* increases, underscoring their strong dependence on the sheet's initial buckling. Here, $\sigma(C_l)$ and $\overline{E_k^*}$ evolve with a similar trend, indicating their strong correlation. Within the SSTM range, both $\sigma(C_l)$ and $\overline{E_k^*}$ experience a first increase and then decrease trend as L^* increases, and when the sheet transitions to DM, a conspicuous decrease in $\sigma(C_l)$ and $\overline{E_k^*}$ is observable.

Figure 7 illustrates the vortex structures generated at some typical moments for various L^* values. Increasing the initial buckling of the sheet $(L^* \rightarrow 0)$ leads to enhanced vortex generation in the wake of the sheet: more intense vortices with more intricate patterns are observed in the downstream channel. Therefore, the vortex generation performance of the VG can be conveniently tuned by altering the sheet's initial buckling. The reason is that a sheet with more pronounced initial buckling protrudes further into the channels (as indicated in figure 6(b), where the oscillation amplitude A^* increases with decreasing L^* values), which is conducive to flow separation and vortex generation. In figure 7, the non-buckled-in channel exhibits developing vortices towards the computational domain's end, rather than the expected decaying ones. This suggests that the vortex intensity varies



Figure 6. Sheet dynamics and associated metrics for varied L^* values. (*a*) Sequentially superimposed sheet profiles. (*b*) Variation of A^* across the range of L^* , delineating two regimes: SSTM and DM. (*c*) Snapping frequencies presented for the SSTM cases. (*d*,*e*) $\overline{C_d}$, $\sigma(C_l)$, $\overline{E_b^*}$ and $\overline{E_k^*}$, plotted against L^* . Additional system parameters: $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $Le^* = 3$ and $m^* = 1$.

throughout the snap-through process, and weaker vortices are generated as the sheet is on the verge of a complete transition from one channel to another.

Figures 8(*a*) and 8(*b*) show the time-averaged flow field for various L^* values, where increased initial buckling introduces greater disturbances in the boundary layer (figure 8*a*) and a larger vertical velocity component (v^*) (figure 8*b*). The v-velocity fluctuation ($\sigma(v^*)$) displayed in figure 8(*c*) demonstrates the flow mixing effect at the four observation points (figure 1). Compared with increasing the bending stiffness K_b^* , increasing the initial buckling of the sheet can more effectively boosts the vortex generation and flow mixing in dual channels: the average $\sigma(v^*)$ value increases by 17 times in the near wake and 4 times in the far wake when L^* is reduced from 0.9 to 0.6. Note that the overall flow mixing effect in the dual channels is assessed by comparing the average $\sigma(v^*)$ values. However,



Figure 7. Vortex generation at different L^* values. Additional parameters: $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $Le^* = 3$ and $m^* = 1$.

it is important to note that this increased flow mixing is accompanied by a larger pressure loss, as depicted in figure 8(d).

3.4. Effects of mass ratio and sheet position

The impact of the mass ratio (m^*) on the sheet dynamics and vortex generation was explored by varying m^* values between 0.5 and 4.0. Additional system parameters, including $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $Le^* = 3$ and $L^* = 0.75$, were considered. Figure 9 displays the superimposed sheet profiles and associated metrics for various m^* values. Our simulations revealed that varying m^* from 0.5 to 4.0 does not trigger any mode transitions, indicating that the sheet mode is insensitive to the variations in mass ratio. This observation is consistent with the experimental findings of Kim *et al.* (2021). Furthermore, our results demonstrate that varying the mass ratio does not significantly impact the vortex generation results and pressure losses, as shown in figures 9(b) and 9(c). These findings suggest that the oscillation and buckling behaviours of the sheet are primarily stiffness-driven phenomena. It appears that the effective stiffness of the sheet, rather than its mass, plays a crucial role in determining the mode and vortex generation capacity of the sheet. The resistance to bending provided by the effective stiffness seems



Figure 8. Characteristics of the flow field and associated metrics for varied K_b^* values. (a,b) Time-averaged vorticity field and v-velocity contours for select K_b^* values. (c) Variation of v-velocity fluctuation $\sigma(v^*)$ in both the near- and far-wake regions of the upper and lower channels. Averaged trends for the near-wake and far-wake regions are indicated with short dashed lines. (d) Evolution of the pressure drop Δp^* across the K_b^* range. Additional system parameters: $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $Le^* = 3$ and $m^* = 1$.



Figure 9. (a) Sequentially superimposed sheet profiles during a snapping cycle for different m^* values. (b,c) $\overline{C_d}$, $\sigma(C_l)$, $\overline{E_b^*}$ and $\overline{E_k^*}$, plotted against m^* . (d,e) Variation of $\sigma(v^*)$ and Δp^* with respect to m^* . Additional parameters: $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $Le^* = 3$ and $L^* = 0.8$.

to be the primary mechanism through which the sheet dynamically interacts with the fluid flow.

In practical applications like cooling electronic chips with a fan, VGs are typically positioned upstream to maximize their influence on the downstream flow. To elucidate the impact of the sheet's positioning on its dynamics and vortex generation performance, we varied the distance from the sheet's leading edge to the inlet, denoted as Le^* , in our simulations. Additionally, for a comprehensive assessment, a simulation incorporating a parabolic inlet velocity profile was also conducted to draw comparisons with the uniform velocity inlet conditions (the mean inlet velocity remains constant between cases). Figure 10(*a*) illustrates the evolution of the boundary layer for $Le^* = 3$. Figure 10(*b*) presents the superimposed sheet profiles at different Le^* values (the parabolic velocity case can be interpreted as the sheet being positioned in a far downstream location where the flow is fully developed). Imposing a parabolic velocity at the inlet transitions the sheet to a dormant mode, highlighting the influence of the boundary layer on the sheet's dynamic behaviour: the developing boundary-layer profiles associated with a uniform velocity inlet exert significantly greater lift and drag forces on the elastic sheet positioned near the wall (figure 10d). This increased force can lead to a higher likelihood of the sheet becoming unstable and undergoing snap-through behaviour. However, increasing the Le* threefold, from 1.8 to 5.4, shows no significant change in the sheet's morphology (figure 10*b*), oscillation amplitude A^* (figure 10*c*), drag coefficient $\overline{C_d}$ (figure 10*d*), v-velocity fluctuation $\sigma(v^*)$ (figure 10*e*) and pressure drop Δp^* (figure 10*f*). This suggests that the flow boundary layer develops gradually in smooth channels, with the sheet's behaviour remaining relatively unaffected by minor variations in the boundary layer. For the SSTM cases, positioning the sheet further downstream increases both its snapping frequency and lift coefficient $\sigma(C_l)$.

3.5. The Reynolds number effect and critical flow conditions

Previous studies (Gomez et al. 2017; Kim et al. 2021a,b) have highlighted the significance of flow strength in initiating the snap-through oscillations of a buckled elastic sheet. In this section, we investigate the effect of *Re* and the critical flow conditions required to trigger SSTM in a dual-channel system. Figure 11 shows the impact of *Re* on the dynamic behaviour of a buckled elastic sheet and its associated metrics within a parametrized system defined by $K_b^* = 5 \times 10^{-3}$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$. A shift from DM to SSTM is observed as *Re* transitions from 500 to 800, as illustrated in figure 11(*a*), underscoring the pivotal role of flow strength in governing the sheet mode. With an increase in Re, we note a limited increase in the oscillation amplitude A^* within SSTM scenarios (figure 11b). The snapping frequency remains approximately constant, near 0.04 (figure 11c), indicating that the snapping amplitude and frequency are not sensitive to flow strength, at least within our considered Re range. An increase in Re correlates with an elevation in $\overline{C_d}$, $\sigma(C_l)$ and $\overline{E_k^*}$ in SSTM cases (figure 11*d*,*e*). Conversely, a decrement in $\overline{E_h^*}$ is noted, which can be attributed to the more flattened sheet profiles generated at larger Re, as illustrated in figure 11(b). Figure 12 presents the flow field characteristics and correlated metrics across a range of *Re*, revealing that at higher *Re*, the VG produces more pronounced vortices and flow perturbations, yet it is associated with a reduced pressure drop. Therefore, the proposed VG demonstrates enhanced performance in higher-*Re* regimes.

Based on the above analysis, it is clear that the sheet mode is primarily influenced by three factors: its initial buckling L^* , bending stiffness K_b^* and the flow strength Re.



Figure 10. (a) Development of boundary layer when the sheet is placed at $Le^* = 3$. (b) Sequentially superimposed sheet profiles, demonstrating morphological changes across different Le^* values. (c) Variation of A^* across the range of Le^* , the inset plots the sheet's snapping frequency. (d) $\overline{C_d}$ and $\sigma(C_l)$, plotted against Le^* . (e) Variation of v-velocity fluctuation $\sigma(v^*)$ in both the near- and far-wake regions of the upper and lower channels. Averaged trends for near-wake and far-wake regions are indicated with short dashed lines. (f) Evolution of the pressure drop Δp^* across the Le^* range. Additional system parameters: $Re_1 = Re_2 = 1000$, $K_b^* = 5 \times 10^{-3}$, $L^* = 0.75$ and $m^* = 1$.

Knowing the critical flow conditions of this system under different L^* and K_b^* values is crucial for its stability and performance optimization. We begin by examining a scenario where both the upper and lower channels have identical flow strengths (i.e. $Re_1 = Re_2$). In the study, the length ratio (L^*) varies from 0.6 to 0.8 and the bending stiffness (K_b^*) ranges



Figure 11. Sheet dynamics and associated metrics for varied *Re*. (*a*) Sequentially superimposed sheet profiles. (*b*) Variation of A^* across the range of *Re*, delineating two regimes: SSTM and DM. (*c*) Snapping frequencies presented for SSTM cases. (*d*,*e*) $\overline{C_d}$, $\sigma(C_l)$, $\overline{E_b^*}$ and $\overline{E_k^*}$ plotted against *Re*. Additional system parameters: $K_b^* = 5 \times 10^{-3}$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$.

from 1.25×10^{-3} to 6.25×10^{-3} . Other parameters considered in our analysis include $Le^* = 3$ and $m^* = 1$.

Figures 13(*a*) and 13(*b*) depict the predicted sheet modes in the parameter spaces of $Re-L^*$ and $Re-K_b^*$, respectively. The dashed lines in these figures indicate the critical Reynolds number (Re_c) necessary for mode transitions. It is apparent that Re_c is significantly dependent on both L^* and K_b^* . An increase in K_b^* leads to a growth in Re_c , suggesting that a higher flow strength is needed to initiate the SSTM of a stiffer sheet, particularly at larger K_b^* values. This finding aligns with the results of Mao *et al.* (2023), where a uniform flow is considered. As L^* increases, an initial decrease in the required Re_c value is observed, reaching a minimum at $L^* = 0.7$, after which it starts to increase, forming a 'V'-shaped curve (figure 13*a*). This indicates that there exists an optimal initial buckling value at which the Re_c needed to trigger snap-through oscillations of the sheet



Figure 12. Characteristics of the flow field and associated metrics for varied *Re*. (*a,b*) Time-averaged vorticity field and v-velocity contours. (*c*) Variation of *v*-velocity fluctuation $\sigma(v^*)$ in both the near- and far-wake regions of the upper and lower channels. Averaged trends for the near-wake and far-wake regions are indicated with short dashed lines. (*d*) Evolution of the pressure drop Δp^* across the *Re* range. Additional system parameters: $K_b^* = 5 \times 10^{-3}$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$.

is minimized. This trend differs from the experimental observations by Kim et al. (2021), where Re_c decreased monotonically with increasing L*. The discrepancy could be due to the smaller Reynolds numbers in our study and our sheet is positioned within or partially within the boundary layer. In the experimental set-up of Kim et al. (2021), higher-Reynolds-numbers flows were considered and their sheet was positioned centrally within a wider channel, thereby the boundary layer effect is minimized. In our simulations, when $L^* < 0.7$, the sheet dynamics is predominantly influenced by the core region flow as the sheet protrudes greatly into the channels. Within this range, the bending energy stored or prestress within the sheet's structure reduces as L^* increases. Consequently, a lesser fluid force suffices to overcome the prestress and initiate snap-through. This accounts for the observed decrement in Re_c with increasing L*. However, for L* values above 0.7, the boundary layer's influence grows. With increasing L^* , the sheet is situated increasingly closer to the sublayer of the boundary layer. Despite the reduction in prestress within the sheet, the fluid forces acting upon it diminish more rapidly, leading to an increment in Re_c as L^* increases. This complex interplay between the prestressed state of the sheet and the fluid dynamic highlights the sensitivity of snap-through phenomena to both the mechanical preconditions of the elastic medium and the characteristics of the surrounding flow field.

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Figure 13. Sheet modes in the parameter spaces of (a) $Re-L^*$ ($K_b^* = 5 \times 10^{-3}$, $Le^* = 3$ and $m^* = 1$) and (b) $Re-K_b^*$ ($L^* = 0.75$, $Le^* = 3$ and $m^* = 1$). The dashed lines represent the critical Reynolds number (Re_c) required to induce a mode transition. (c) Re_c plotted in the parameter spaces of $L^*-K_b^*$ ($Le^* = 3$ and $m^* = 1$).

Figure 13(c) illustrates the predicted Re_c value across the parameter space defined by the length ratio (L^*) and the bending stiffness (K_b^*), with the sheet position at $Le^* = 3$ and the mass ratio fixed at $m^* = 1$. It is observed that irrespective of the L^* values surveyed, Re_c increases with increasing bending stiffness and the increase in Re_c is more pronounced at higher K_b^* values. For the examined K_b^* values, the required Re_c values experience an initial escalation followed by a subsequent decline as L^* increases, with the minimum Re_c value obtained always at approximately $L^* = 0.7$. Additionally, the impact of L^* on Re_c becomes more significant at higher K_b^* values.

We then consider the scenario where the upper and lower channels exhibit different flow strengths (i.e. $Re_1 \neq Re_2$). The flow strength of the lower channel is fixed at $Re_1 = 1000$, with a corresponding flow velocity $U_1 = 0.012$. The incoming flow velocity of the upper channel (U_2) is varied to obtain the desired velocity disparity U_1/U_2 between the upper and lower channels. In figure 14(*a*), we presented the superimposed sheet profiles under varied U_1/U_2 ratios. When a sheet undergoes the SSTM, its superimposed profile becomes

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Figure 14. (a) Superimposed sheet profiles under varied U_1/U_2 ratios, with $K_b^* = 3.75 \times 10^{-3}$, $L^* = 0.75$, $Le^* = 3$ and $m^* = 1$. (b) Critical U_1/U_2 ratios in the parameter space of $L^* - K_b^*$ when Re_1 is fixed at 1000. (c) Comparison of the critical Re_2 required for mode transition under conditions $Re_1 = Re_2$ and $Re_1 = 1000$. Additional parameters: $Le^* = 3$ and $m^* = 1$.

asymmetrical when $U_1/U_2 \neq 1$. In this case, the lower half of the profiles deflects more in the streamwise direction due to the higher flow strength in the lower channel. Additionally, the snap-through process is more challenging and time-consuming when the sheet snaps from the upper channel (lower Re) to the lower channel (higher Re). If the velocity ratio U_1/U_2 exceeds a critical value, the sheet enters a DM in the channel with lower flow strength. Figure 14(b) shows the critical U_1/U_2 ratios in the parameter space of $L^*-K_h^*$ when Re_1 is fixed at 1000. The critical U_1/U_2 ratio increases with decreasing K_h^* value, indicating that larger velocity disparity is permissible for inducing the SSTM of more compliant sheets. As L^* increases, the critical U_1/U_2 ratio initially escalates and then declines. Therefore, a larger velocity disparity is also allowed for medium initial buckling. Figure 14(b) compares the critical Re_2 required to induce a mode transition in two scenarios: $Re_1 = Re_2$ and $Re_1 \neq Re_2$ (with $Re_1 = 1000$). It is found that when the lower channel flow is fixed at $Re_1 = 1000$, a larger Re_2 is required to initiate the SSTM of the sheet. This suggests that the flow strength disparity between the two channels suppresses the snap-through of the sheet. To harness the sheet's snap-through for enhanced vortex generation in dual-channel flow, the disparity in flow strengths between the channels should be minimized.

4. Conclusions

This study presents a novel flexible vortex generator (VG) specifically designed for dual-channel flow configurations. Unlike traditional flapping flag-type VGs, the proposed design harnesses the snap-through behaviour of a buckled elastic sheet with two clamped ends. The dynamics and vortex generation performance of the sheet under various system parameters are numerically investigated using the immersed boundary-lattice Boltzmann method. The major findings are summarized below.

Compared with a rigid VG of similar size, the proposed VG can effectively generate vortices in both channels, resulting in improved overall flow mixing and reduced pressure loss. Varying system parameters reveal two distinct sheet modes: a sustained snap-through mode (SSTM) and a dormant mode (DM). The sheet, exhibiting regular SSTM, can effectively generate vortices in both channels, especially with a larger initial buckling

https://doi.org/10.1017/jfm.2024.244 Published online by Cambridge University Press

and in higher Reynolds number regimes. For a given system, the vortex generation performance of the VG can be conveniently tuned by altering the sheet's initial buckling.

The sheet's mode is primarily influenced by its length ratio (L^*), bending stiffness (K_h^*) and the flow strength (Re), with the mass ratio of the sheet playing a marginal role. This suggests that the oscillation of the sheet is primarily a stiffness-driven phenomenon, and varying L^* , K_h^* and Re can alter the sheet's effective stiffness. An increase in K_h^* leads to a growth in the critical Reynolds number (Re_c) required for mode transition, with a more significant growth rate at larger K_h^* values. Consequently, a higher flow strength is necessary to initiate the SSTM of a stiffer sheet. As the initial buckling increases (i.e. L^* decreases), the required Re_c initially escalates, followed by a subsequent decline, suggesting an optimal length ratio L^* (approximately 0.7 for our considered system) at which SSTM can be more easily triggered. This trend may be due to the nuanced interplay between the prestressed state of the sheet and the fluid dynamic environment, especially the boundary layer effect. When the upper and lower channels have different flow strengths, the sheet exhibits asymmetrical dynamics, deflecting more significantly and spending less time in the channel with stronger flow strength. Additionally, a disparity in flow strength between the upper and lower channels is found to inhibit the snap-through behaviour of the sheet; thus, the disparity should be minimized in such systems. A larger disparity in flow strength is permissible to induce SSTM in more compliant sheets and those with medium initial buckling.

This research opens new avenues for optimizing flow control strategies in dual-channel flow set-ups. The results highlight the immense potential of harnessing snap-through behaviour in elastic sheets as a highly effective method for achieving improved flow manipulation and vortex generation. In our future work, we aspire to incorporate heat transfer modules into our algorithms. This extension will enable us to investigate the enhanced heat transfer effects of our proposed vortex generator within the context of a dual-channel system.

Supplemental movies. Supplementary movies are available at https://doi.org/10.1017/jfm.2024.244.

Funding. This work was supported by National Natural Science Foundation of China (grant nos. 12202393, 51976200 and 11872062); Natural Science Foundation of Zhejiang Province (grant no. LTGY23A020001).

Declaration of interests. The authors report no conflict of interest.

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REFERENCES

- AKCAYOGLU, A. & NAZLI, C. 2018 A comprehensive numerical study on thermohydraulic performance of fluid flow in triangular ducts with delta-winglet vortex generators. *Heat Transfer Engng* 39, 107–119.
- ARNOUTS, L.I.W., MASSART, T.J., DE TEMMERMAN, N. & BERKE, P.Z. 2019 Computational design of bistable deployable scissor structures: trends and challenges. J. Intl Assoc. Shell Spatial Struct. 60, 19–34.
- AWAIS, M. & BHUIYAN, A.A. 2018 Heat transfer enhancement using different types of vortex generators (VGs): a review on experimental and numerical activities. *Therm. Sci. Engng Prog.* 5, 524–545.
- BHARADWAJ, P., KHONDGE, A.D. & DATE, A. 2009 Heat transfer and pressure drop in a spirally grooved tube with twisted tape insert. *Intl J. Heat Mass Transfer* **52**, 1938–1944.
- BHATTACHARYYA, S. 2020 Fluid flow and heat transfer in a heat exchanger channel with short-length twisted tape turbulator inserts. *Iran. J. Sci. Technol.* 44, 217–227.
- BOBBERT, F.S.L., JANBAZ, S. & ZADPOOR, A.A. 2018 Towards deployable meta-implants. J. Mater. Chem. B 6, 3449–3455.

CAI, G., XUE, L., ZHANG, H. & LIN, J. 2017 A review on micromixers. Micromachines 8 (online).

- CAO, Y.T., DERAKHSHANI, M., FANG, Y.H., HUANG, G.L. & CAO, C.Y. 2021 Bistable structures for advanced functional systems. Adv. Funct. Mater. 31, 2106231.
- CHEN, Y., YANG, J., LIU, Y. & SUNG, H.J. 2020 Heat transfer enhancement in a poiseuille channel flow by using multiple wall-mounted flexible flags. *Intl J. Heat Mass Transfer* **163**, 120447.
- CHEN, Y.J., YU, Y.L., PENG, D. & LIU, Y.Z. 2019 Heat transfer enhancement of turbulent channel flow using dual self-oscillating inverted flags: staggered and side-by-side configurations. *Intl J. Heat Mass Transfer* 136, 851–863.
- CONNELL, B.S. & YUE, D.K. 2007 Flapping dynamics of a flag in a uniform stream. J. Fluid Mech. 581, 33–67.
- CUI, J., LIN, Z., JIN, Y. & LIU, Y. 2019 Numerical simulation of fiber conveyance in a confined channel by the immersed boundary-lattice Boltzmann method. *Eur. J. Mech.* (B/Fluids) 76, 422–433.
- CUI, J., LIU, Y. & JIN, Y. 2021 Impact of initial fiber states on different fiber dynamic patterns in the laminar channel flow. Intl J. Mech. Sci. 198, 106359.
- CUI, J., WANG, Z., LIU, Y., JIN, Y. & ZHU, Z. 2022a Three-dimensional simulation of lateral migration of fiber in a laminar channel flow. *Intl J. Mech. Sci.* 236, 107766.
- CUI, J., WU, T., LIU, Y., FU, B.M., JIN, Y. & ZHU, Z. 2022b A three-dimensional simulation of the dynamics of primary cilia in an oscillating flow. *Appl. Math. Model.* 108, 825–839.
- CURRIER, T.M., LHERON, S. & MODARRES-SADEGHI, Y. 2020 A bio-inspired robotic fish utilizes the snap-through buckling of its spine to generate accelerations of more than 20 g. *Bioinspir. Biomim.* 15, 055006.
- DONG, H.X., CHEN, C.Y., QIU, C., YEOW, C.H. & YU, H.Y. 2022 GSG: a granary-shaped soft gripper with mechanical sensing via snap-through structure. *IEEE Robot. Autom. Lett.* 7, 9421–9428.
- GALLEGOS, R.K.B. & SHARMA, R.N. 2017 Flags as vortex generators for heat transfer enhancement: gaps and challenges. *Renew. Sustain. Energy Rev.* 76, 950–962.
- GOMEZ, M., MOULTON, D.E. & VELLA, D. 2017 Passive control of viscous flow via elastic snap-through. *Phys. Rev. Lett.* 119, 144502.
- GORISSEN, B., MELANCON, D., VASIOS, N., TORBATI, M. & BERTOLDI, K. 2020 Inflatable soft jumper inspired by shell snapping. Sci. Robot. 5, eabb1967.
- HAN, J.C., GLICKSMAN, L.R. & ROHSENOW, W.M. 1978 An investigation of heat transfer and friction for rib-roughened surfaces. *Intl J. Heat Mass Transfer* 21, 1143–1156.
- HE, Y.L., HAN, H., TAO, W.Q. & ZHANG, Y.W. 2012 Numerical study of heat-transfer enhancement by punched winglet-type vortex generator arrays in fin-and-tube heat exchangers. *Intl J. Heat Mass Transfer* 55, 5449–5458.
- HUA, R.-N., ZHU, L. & LU, X.-Y. 2013 Locomotion of a flapping flexible plate. Phys. Fluids 25, 121901.
- HUANG, Q., LAI, J.C.S., TIAN, F.-B. & YOUNG, J. 2021 Transition to chaos in a two-sided collapsible channel flow. J. Fluid Mech. 926, A15.
- HUANG, W.-X., SHIN, S.J. & SUNG, H.J. 2007 Simulation of flexible filaments in a uniform flow by the immersed boundary method. J. Comput. Phys. 226, 2206–2228.
- HUSSAIN, A.A., FREEGAH, B., KHALAF, B.S. & TOWSYFYAN, H. 2019 Numerical investigation of heat transfer enhancement in plate-fin heat sinks: effect of flow direction and fillet profile. *Case Stud. Therm. Engng* 13, 100388.
- JEONG, C.H., KIM, H.R., HA, M.Y., SON, S.W., LEE, J.S. & KIM, P.Y. 2014 Numerical investigation of thermal enhancement of plate fin type heat exchanger with creases and holes in construction machinery. *Appl. Therm. Engng* 62, 529–544.
- JIAO, S. & LIU, M. 2021 Snap-through in graphene nanochannels: with application to fluidic control. ACS Appl. Mater. Interfaces 13, 1158–1168.
- KANG, S.K. 2010 Immersed boundary methods in the lattice Boltzmann equation for flow simulation. Doctor Thesis, Texas A&M University.
- KHATAVKAR, V.V., ANDERSON, P.D., DEN TOONDER, J.M.J. & MEIJER, H.E.H. 2007 Active micromixer based on artificial cilia. *Phys. Fluids* 19, 083605.
- KIM, B.S., KWAK, B.S., SHIN, S., LEE, S., KIM, K.M., JUNG, H.-I. & CHO, H.H. 2011 Optimization of microscale vortex generators in a microchannel using advanced response surface method. *Intl J. Heat Mass Transfer* 54, 118–125.
- KIM, H., LAHOOTI, M., KIM, J. & KIM, D. 2021a Flow-induced periodic snap-through dynamics. J. Fluid Mech. 913, A52.
- KIM, H., ZHOU, Q., KIM, D. & OH, I.-K. 2020 Flow-induced snap-through triboelectric nanogenerator. Nano Energy 68, 104379.
- KIM, J., KIM, H. & KIM, D. 2021b Snap-through oscillations of tandem elastic sheets in uniform flow. J. Fluids Struct. 103, 103283.

- LAMBERT, R.A. & RANGEL, R.H. 2010 The role of elastic flap deformation on fluid mixing in a microchannel. *Phys. Fluids* **22**, 052003.
- LEE, C.-Y., WANG, W.-T., LIU, C.-C. & FU, L.-M. 2016 Passive mixers in microfluidic systems: a review. Chem. Engng J. 288, 146–160.
- LEE, J.B., PARK, S.G., KIM, B., RYU, J. & SUNG, H.J. 2017 Heat transfer enhancement by flexible flags clamped vertically in a Poiseuille channel flow. *Intl J. Heat Mass Transfer* 107, 391–402.
- LEE, J.B., PARK, S.G. & SUNG, H.J. 2018 Heat transfer enhancement by asymmetrically clamped flexible flags in a channel flow. *Intl J. Heat Mass Transfer* **116**, 1003–1015.
- LIAO, W. & JING, D. 2023a Experimental study on fluid mixing and pressure drop of mini-mixer with flexible vortex generator. *Intl Commun. Heat Mass Transfer* 142, 106615.
- LIAO, W. & JING, D.L. 2023b Experimental study on fluid mixing and pressure drop of mini-mixer with flexible vortex generator. Intl Commun. Heat Mass Transfer 142, 106615.
- LUO, X.Y., CAI, Z.X., LI, W.G. & PEDLEY, T.J. 2008 The cascade structure of linear instability in collapsible channel flows. J. Fluid Mech. 600, 45–76.
- MAHMOODI-JEZEH, S.V. & WANG, B.C. 2020 Direct numerical simulation of turbulent flow through a ribbed square duct. J. Fluid Mech. 900, A18.
- MAO, Q., LIU, Y. & SUNG, H.J. 2023 Snap-through dynamics of a buckled flexible filament in a uniform flow. J. Fluid Mech. 969, A33.
- MOORE, A.L. & SHI, L. 2014 Emerging challenges and materials for thermal management of electronics. *Mater. Today* 17, 163–174.
- NIU, X.D., SHU, C., CHEW, Y.T. & PENG, Y. 2006 A momentum exchange-based immersed boundary-lattice Boltzmann method for simulating incompressible viscous flows. *Phys. Lett.* A 354, 173–182.
- PARK, S.G., KIM, B., CHANG, C.B., RYU, J. & SUNG, H.J. 2016 Enhancement of heat transfer by a self-oscillating inverted flag in a Poiseuille channel flow. *Intl J. Heat Mass Transfer* 96, 362–370.
- PESKIN, C. 2002 The immersed boundary method. Acta Numerica 11, 479–517.
- PREMNATH, K. & ABRAHAM, J. 2007 Three-dimensional multi-relaxation time (MRT) lattice-Boltzmann models for multiphase flow. J. Comput. Phys. 224, 539–559.
- PROMVONGE, P. & THIANPONG, C. 2008 Thermal performance assessment of turbulent channel flows over different shaped ribs. *Intl Commun. Heat Mass Transfer* 35, 1327–1334.
- QIN, W.Y., DENG, W.Z., PAN, J.N., ZHOU, Z.Y., DU, W.F. & ZHU, P. 2019 Harvesting wind energy with bi-stable snap-through excited by vortex-induced vibration and galloping. *Energy* 189, 116237.
- SHOELE, K. & MITTAL, R. 2014 Computational study of flow-induced vibration of a reed in a channel and effect on convective heat transfer. *Phys. Fluids* 26, 127103.
- SINGH, G. & LAKKARAJU, R. 2019 Wall-mounted flexible plates in a two-dimensional channel trigger early flow instabilities. *Phys. Rev.* E 100, 023109.
- SKULLONG, S., PROMTHAISONG, P., PROMVONGE, P., THIANPONG, C. & PIMSARN, M. 2018 Thermal performance in solar air heater with perforated-winglet-type vortex generator. *Solar Energy* 170, 1101–1117.
- TANDA, G. 2011 Performance of solar air heater ducts with different types of ribs on the absorber plate. *Energy* 36, 6651–6660.
- WANG, C. & TANG, H. 2018 Influence of complex driving motion on propulsion performance of a heaving flexible foil. *Bioinspir. Biomim.* 14, 016011.
- WANG, C. & TANG, H. 2019 On the aeroelastic energy transfer from a Lamb dipole to a flexible cantilever. J. Fluids Struct. 86, 170–184.
- WANG, C.L., TANG, H., DUAN, F. & YU, S.C.M. 2016a Control of wakes and vortex-induced vibrations of a single circular cylinder using synthetic jets. J. Fluids Struct. 60, 160–179.
- WANG, C.L., TANG, H., YU, S.C.M. & DUAN, F. 2016b Active control of vortex-induced vibrations of a circular cylinder using windward-suction-leeward-blowing actuation. *Phys. Fluids* 28, 14.
- WANG, C.L., TANG, H., YU, S.C.M. & DUAN, F. 2017a Control of vortex-induced vibration using a pair of synthetic jets: influence of active lock-on. *Phys. Fluids* 29, 11.
- WANG, C.L., TANG, H., YU, S.C.M. & DUAN, F. 2017b Lock-on of vortex shedding to a pair of synthetic jets with phase difference. *Phys. Rev. Fluids* 2, 26.
- WANG, Y.S., ZHOU, Z.Y., QIN, W.Y. & ZHU, P. 2021 Harvesting wind energy with a bi-stable configuration integrating vortex-induced vibration and galloping. J. Phys. D-Appl. Phys. 54, 285501.
- WANG, Z., ZHAO, F., FU, Y., DENG, F., ZENG, L. & CUI, J. 2023 Towards energy harvesting through flow-induced snap-through oscillations. *Intl J. Mech. Sci.* 254, 108428.
- WEBB, R.L., ECKERT, E.R.G. & GOLDSTEIN, R.J. 1971 Heat transfer and friction in tubes with repeated-rib roughness. Intl J. Heat Mass Transfer 14, 601–617.
- WIENS, J.K. & STOCKIE, J.M. 2015 Simulating flexible fiber suspensions using a scalable immersed boundary algorithm. *Comput. Meth. Appl. Mech. Engng* 290, 1–18.

- WU, J.F., LIU, P., YU, M.J., LIU, Z.C. & LIU, W. 2022b Thermo-hydraulic performance and exergy analysis of a fin-and-tube heat exchanger with sinusoidal wavy winglet type vortex generators. *Intl J. Therm. Sci.* 172, 107274.
- WU, S., BAKER, G.L., YIN, J. & ZHU, Y. 2022a Fast thermal actuators for soft robotics. Soft Robot. 9, 1031–1039.
- YANG, X., ZHANG, X., LI, Z. & HE, G.-W. 2009 A smoothing technique for discrete delta functions with application to immersed boundary method in moving boundary simulations. J. Comput. Phys. 228, 7821–7836.
- YEOW, B.S., et al. 2021 Origami-inspired snap-through bistability in parallel and curved mechanisms through the inflection of degree four vertexes. In IEEE International Conference on Robotics and Automation (ICRA), May 30–June 05 2021 Xian, People's Republic of China, pp. 10863–10869.
- YU, Y.L., LIU, Y.Z. & CHEN, Y.J. 2018 Vortex dynamics and heat transfer behind self-oscillating inverted flags of various lengths in channel flow. *Phys. Fluids* 30, 045104.
- YUAN, H.-Z., NIU, X.-D., SHU, S., LI, M. & YAMAGUCHI, H. 2014 A momentum exchange-based immersed boundary-lattice Boltzmann method for simulating a flexible filament in an incompressible flow. *Comput. Maths Applics.* 67, 1039–1056.
- ZHANG, X.J., OSEYEMI, A.E., MA, K. & YU, S.Y. 2022 Entirely soft valve leveraging snap-through instability for passive flow control. *Sensors Actuators* B-*Chem.* 367, 132035.
- ZHANG, Z., WANG, X. & YAN, Y. 2021 A review of the state-of-the-art in electronic cooling. *e-Prime Adv. Electr. Engng Electron. Energy* 1, 100009.
- ZHAO, J., HUANG, S.B., GONG, L. & HUANG, Z.Q. 2016 Numerical study and optimizing on micro square pin-fin heat sink for electronic cooling. *Appl. Therm. Engng* 93, 1347–1359.
- ZHOU, G.B. & FENG, Z.Z. 2014 Experimental investigations of heat transfer enhancement by plane and curved winglet type vortex generators with punched holes. *Intl J. Therm. Sci.* **78**, 26–35.
- ZHOU, Z., QIN, W., ZHU, P., DU, W., DENG, W. & PAN, J. 2019 Scavenging wind energy by a dynamic-stable flutter energy harvester with rectangular wing. *Appl. Phys. Lett.* **114**, 243902.